Investigation of Swirling and Tumbling Flow Pattern of Spark Ignition Engine

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Abstract
Gas motion within the cylinder is one of the major factors that control the combustion process in spark ignition engine. It also has significant impact on heat transfer. Both the bulk gas motion and the turbulence characteristics of the flow are important and governing the overall behavior of the flow. An arrangement for obtaining a stratified charge, using port injection, is proposed for a current design of a spark ignition engine. The behavior of combustion are simulated with Computational fluid dynamic and tested. Engine testing was performed using dynamometer for measuring the lean burn limit of the current spark ignition engine. Some concepts for premixed lean burn are introduced during the previous decade and with this state of the art concept the swirl and tumble flow pattern can generate in each speed, therefore the effect of these pattern on lean burn limit is investigated.

Keywords: Swirl Flow Pattern, Tumble FlowPattern, Lean Burn, Brake Specific Fuel Consumption, Brake Mean Effective Pressure

1. Introduction
Charge stratification is an effective measure to extend lean burn or EGR limits in spark ignition engines and therefore gives an increased fuel economy and decreased NOx and CO2 emissions. It can be achieved by means of strong large-scale air flow (swirl, tumble or inclined-axis swirl), but different company use different flow pattern to achieve more stable combustion for example: Mitsubishi [1 and 2] and Subaru adopt tumble as the large scale eddy to preserve the energy. Honda [3] adopts swirl, and Toyota [4 and 5], Nissan [6] and Mazda [7] adopt so-called inclined swirl, that is the flow combined tumble and swirl.

For investigation the flow pattern three models are tested, base line-engine, port with flow control baffle No. 1 (block
half of the port entrance, see fig. 1) and finally port with flow control baffle No. 2 (block the entire one intake valve, see fig. 1).

With the first flow control baffle, the part of the intake port entrance is blocked so the flow during entering the cylinder rotates and produces different bulk motion, swirl (Fig. 1), and with another flow control baffle the entire of one of the intake valve (from two intake valves) is covered (Fig. 1).

Fig. 1. Flow control baffles

The experimental tests and engine simulation were done at an engine operating condition of 2000 rev/min, 2 bar Brake mean effective pressure (BMEP). Motored tests are conducted on a four valves, four cylinders engine with geometric characteristics summarized in table 1.

TABLE 1. Engine specification

<table>
<thead>
<tr>
<th>Fuel type</th>
<th>Gasoline</th>
</tr>
</thead>
<tbody>
<tr>
<td>Bore × Stroke (mm×mm)</td>
<td>83 × 72</td>
</tr>
<tr>
<td>Displacement (cm³)</td>
<td>1400</td>
</tr>
<tr>
<td>Bore (mm)</td>
<td>78.6</td>
</tr>
<tr>
<td>Compression ratio</td>
<td>10.5</td>
</tr>
<tr>
<td>IVO/IVC</td>
<td>39 °BTDC/64 °ABDC</td>
</tr>
<tr>
<td>EVO/EVC</td>
<td>17 °BBDC/9 °ATDC</td>
</tr>
</tbody>
</table>

2. Experimental Procedure

Swirl and tumble ratios are usually measured in a steady flow rig for a given valve lift. A torque meter is used to quantify the charge motion torque. To measure swirl, the torque meter is mounted at the bottom of the cylinder. The air flow is sucked up through the inlet port, to simulate the operation of a naturally aspirate engine. Unlike swirl, the generation of tumbling motion is not only outflow characteristics of the intake system but also the impinging on the piston. Thus the specific design is required to take into account the piston effect. The tumble ratio values so determined are specific of the design of the tumble rig and cannot be directly compared to data obtained from other tumble rigs (Fig. 2). For the steady state flow rig, the swirl ratio and tumble ratio are defined as below:

\[ C_s = \frac{8T}{m v_c B} \]  

\[ (1) \]

where \( T \) is the torque and \( m v_c \) is the air mass flow rate and the bore (B) has been used as characteristic dimension. The velocity is defined by:

\[ v_v = \left( \frac{2(P_s - P)}{\rho} \right)^{0.5} \]

\[ (2) \]

\( (P_s - P) \) is the pressure drop across the valve using an incompressible flow equation. For the CFD calculation, the swirl ratio \( R_s \) (and Tumble ratio \( R_t \)) is defined as the ratio of the angular velocity of in-cylinder flow to the engine angular velocity \( N \):

\[ R_s = \omega / N \]

\[ (3) \]

The device that is shown figure 4 is used to measure the injector parameters.

The sprayed quantity is collected and measured separately for each of the 8 segments in a measuring insert shown in fig. 4. The results of the test for calibration the injector model is shown in table 2.

TABLE 2. Injector specification

<table>
<thead>
<tr>
<th>S</th>
<th>X</th>
<th>Y</th>
<th>Z</th>
<th>D</th>
<th>Q(stat)</th>
<th>Q(dyn)</th>
</tr>
</thead>
<tbody>
<tr>
<td>15</td>
<td>28</td>
<td>7</td>
<td>17.6</td>
<td>36.4</td>
<td>100</td>
<td>158.2</td>
</tr>
</tbody>
</table>
3. CFD modeling

All CFD calculations were performed using VECTIS\(^1\). The code is characterized by the feature of automatic generation of computational grid based on the cut cell technique for wall surfaces. Due to the fact that it is automatic, the labour required for mesh generation is relatively low and the method can be incorporated into the flow of the engine development cycle that usually has strict time constraints.

Fundamental equations are first discretised using the finite volume method, and then solved fully-implicitly, with coupling between variables and non-linear effects incorporated using iterative or predictor corrector methods. Transient or steady flows can be calculated.

The effect of turbulence is represented by the k-ε model. In the k-ε model, the molecular diffusivity for each transported variable is augmented by a turbulent diffusivity calculated from the turbulent kinetic energy (k) and its dissipation rate (ε), for which additional transport equations are solved. To avoid degeneracy problems, The PISO algorithm is used to couple the pressure and velocity for both compressible and incompressible flows.

The initial conditions inside the cylinder was assumed to be an inert gas with the cylinder pressure and temperature at intake TDC. The boundary conditions with and without flow control baffles are extracted from experimental tests.

The 2-phase spray model accounts for full interaction between the gas and liquid phases.

Fuel sprays are treated as a dispersed liquid phase, which moves in and interacts with the surrounding continuous gas phase. A fuel spray is represented by an ensemble of discrete droplet “parcels”, each parcel containing a number of droplets with the same size, velocity and temperature. The droplet parcel is tracked in a Lagrangian fashion as they move through the gas phase, exchanging mass, momentum and energy. The affect of the droplet parcels on the continuous phase due to drag, heat and mass transfer is implemented via source terms in the gas phase conservation equations.

Sub models are provided for droplet break up, coalescence, turbulence interaction, wall impingement and re-entrainment.

The momentum equation for a droplet of mass \(md\) is described by Newton’s Law:

\[
m_d \frac{dU_d}{dt} = \frac{1}{2} C_d \rho A_d \left| U - U_d (U - U_d) \right|
\]

where \(C_d\) is the drop drag coefficient, \(\rho\) is the gas density and \(A_d\) is the drop frontal area.

The drag force depends on the relative velocity between ambient and drop:

\[
U_r = U - U_d
\]

The drag coefficient suggested by Putnam [9] is used for the trajectory calculation:

\[
C_d = \begin{cases} 
\frac{24}{Re_d} & (Re_d \leq 1000) \\
1 + \frac{1}{6} Re_d^{\frac{2}{3}} & (Re_d \geq 1000) \\
0.424 & 
\end{cases}
\]

The drop Reynolds number is defined as:

\[
Re_d = \left( \rho U_r D_r \right)/\mu
\]

where \(\mu\) is the gas dynamic viscosity. This empirical formula is suitable for numerical integration and has demonstrated reasonably accuracy against experimental data. When Reynolds numbers tend to zero, the formula becomes the Stokes Law, i.e.

\[
C_d = 24/Re_d
\]

For high Reynolds numbers, the drag coefficient approaches a stable value.

The evaporation of drops in a spray involves simultaneous heat and mass transfer processes. The heat for evaporation is transferred to the drop surface by convection and conduction from the surrounding gas, the vapour is transferred back to the gas stream by convection and diffusion. The droplet mass and temperature are calculated from the Eqs. [10] and [11] as below:

\[
\frac{dm_d}{dt} = -A_d Sh \frac{D_{AB}}{D_d} \rho_v \ln \left( \frac{P - P_{v,\infty}}{P - P_{v,s}} \right)
\]

\[
m_d \frac{dC_{p,d} T_d}{dt} = -A_d N u (T_d - T) K_m F_z + h_\text{fg} \frac{dm_d}{dt}
\]

where \(D_{AB}\) is the mass diffusivity, \(K_m\) is the mixture thermal conductivity, \(C_{p,d}\), is the specific heat of liquid fuel, \(h_\text{fg}\) is the latent heat of evaporation, \(P\) is the pressure of gas mixture, and \(P_{v,f}\) and \(P_{v,s}\) stand for the partial pressure at the drop surface and ambient, respectively.

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\(1\) CFD package from Ricardo Company

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The fuel vapour density \( \rho_f \) is evaluated from the gas pressure and mean temperature,

\[
T_m = \frac{(T_d + T)}{2}
\]  
(10)

The Sherwood and Nusselt numbers, \( Sh \) and \( Nu \), are calculated by the correlation by Ranz and Marshall [12]:

\[
Sh = 2 \left( 1 + 0.3 \frac{Re_D}{Sc} \right) \frac{1}{1}
\]

\[
Nu = 2 \left( 1 + 0.3 \frac{Re_D}{Pr} \right) \frac{1}{1}
\]  
(11)

A gasoline atomization model developed at the Engine Research Centre of Wisconsin University [13] to predict the atomization conditions of gasoline injectors with reasonable accuracy. This model contains two elements: the first is concerned with estimating the initial thickness and velocity of the liquid sheet at the orifice exit and the sheet breakup length, given that the injection pressure, injection mass flow rate, and orifice diameter are known; the second involves representing the continuous sheet as a number of discrete blobs and evaluating their primary breakup processes using the TAB (Taylor-Analogy Breakup) breakup model [14].

The model of Gosman and Bai is used to model the injector behaviour for different regimes of wall roughness, fuel and wall temperature, impingement angle and speed etc.

As the liquid phase is numerically modelled using the Lagrangian approach, injection of continuous conical liquid sheet at the injector is effected by introducing a number of blobs, or parent droplet parcels, at each computational time step, each with a diameter equal to the initial sheet thickness and velocity respectively, at the corresponding injection time. Each blob has a lifetime equal to its breakup time during which it experiences no air drag and has no interaction with other blobs or droplets. The atomization of each blob is calculated according to the TAB model. In this, an oscillating and distorting droplet is viewed as a mass-spring system, in which the external force acting on the mass, the restoring force of the spring and the damping force are taken in an analogous way as aerodynamic force exerted on the droplet, surface tension force and droplet viscous force respectively. Thus, a forced and harmonic oscillation of the droplet is described by the following equation:

\[
\frac{d^2 y}{dt^2} + \frac{5 \mu_l}{\rho_l r_b^2} \frac{dy}{dt} + \frac{8 \sigma}{\rho_1 r_b^3} - \frac{2 \rho_s U^2}{3 \rho_1 r_b^3} = 0
\]  
(12)

where \( y \) is droplet oscillation parameter scaled with the blob radius \( r_b \), \( \rho_s \) and is the ambient gas density. The criterion for droplet breakup is \( y > 1 \). Once this condition is reached, the droplet starts to disintegrate into a collection of small droplets which are assumed to observe Rosin-Rammler distribution described by:

\[
f(D) = \frac{q D^{q-1}}{\bar{D}^q} \exp \left[ -\left( \frac{D}{\bar{D}} \right)^q \right]
\]  
(13)

Where \( \bar{D} \) is related to the Sauter mean diameter \( D_{32} \) as:

\[
\bar{D} = D_{32} \Gamma \left( 1 - \frac{1}{q} \right)
\]  
(14)

To evaluate \( D_{32} \), energy balance before and after breakup is invoked to give:

\[
D_{32} = 2 \rho_0 \left[ \frac{7}{3} + \frac{\rho_1 r_b^3 (dy/dt)^2}{8 \sigma} \right]^{-1}
\]  
(15)

For fuel droplet impingement, liquid which sticks to the wall becomes a film. Heat and mass transfer of the wall film is calculated, so that fuel which impinges on the wall can evaporate from the wall and rejoin the calculation. Models that are used in this study are listed in table 3.

<table>
<thead>
<tr>
<th>TABLE 3: Simulation characteristics</th>
<th>Models</th>
</tr>
</thead>
<tbody>
<tr>
<td>Gasoline Atomization ERC</td>
<td></td>
</tr>
<tr>
<td>Droplet Break up TAB ( Taylor Analogy Breakup)</td>
<td></td>
</tr>
<tr>
<td>Wall roughness Gosman and Bai</td>
<td></td>
</tr>
<tr>
<td>Sherwood and Nusselt Number Ranz and Marshal</td>
<td></td>
</tr>
</tbody>
</table>

4. Results and discussions

Tumble ratio curves measured on the steady flow bench are presented in fig. 3 as a function of valve lift, for the various flow control baffles. For the base line-engine configuration without baffle between cylinder head and intake manifold, no significant swirling motion is induced. (Fig. 4)

For base line engine, two bulk swirl are generated but in opposite direction as the result of port shape. Because of this matter the swirl meter test rig shows the zero torque for swirling motion (as we expected for engine with two similar intake valves). Tumble ratio that is measured in the steady flow rig is shown in Figs. 5 and 6.

For base line engine two swirling motion are generated in opposite direction therefore no significant swirling motion is induced and measured in Swirl meter.

Fig. 6 shows the evolution of swirl ratio in function of the valve lift for different flow control baffles.

Tumble ratio of three configurations is the same but swirl ration differ a lot between configurations.

By using CFD calculation the trend of Tumbling motion and swirling motion versus crank angle is investigated

Swirl ratio measured by CFD calculation is presented in Fig. 7.
Fig. 4 shows the evolution of swirl ratio in function of the valve lift for different flow control baffles.

Fig. 5. Tumble ratio with various flow-controls baffles designs

From Fig. 7, it is observed that the swirling motion of flow control baffle Nos. 1 and 2 is existed up to the end of compression stroke. In base line engine, two opposite swirl is generated that canceled each other in the total volume of the cylinder (fig. 8). In all the figs. 0 is TDC of gas exchange. It is notable that the swirl ratio based on the steady state test rig for baffle No.2 is higher than baffle No.1 (fig. 4) but as shown in fig. 7 this matter is not true completely. [8]

Tumble ratio in two other axes is presented in Figs 9 and 10. The tumble ratio of both control baffles is higher than base line engine and the behaviors of tumble ratio in both axes of control baffles are the same.

In this paper the total rotation ratio is defined as:

\[
\text{Rotation ratio} = R_{s1}^2 + R_{s2}^2 + R_{sk}^2
\]  

(16)

The rotation ratio is presented in fig. 9. The rotation ratio of flow control baffle No.1 is higher than the control baffle No. 2. The rotation ratio of two control baffles is higher than the base-line engine.
5. Experimental results

Lean burn limit can be judged from the relations of coefficient of variation (COV) in indicated mean effective pressure (IMEP) versus air/fuel ratio at part load condition. For base line engine, the maximum COV of IMEP occurs in cylinder No. 4 and for flow control baffles Nos. 1 and 2, it occurs in cylinder No. 4. Because of various flow fields and different temperature of cylinders, the COV of IMEP of cylinders is not the same, the maximum COV of IMEP is occurred in cylinder number as shown in Table 3 and Fig. 12.

<table>
<thead>
<tr>
<th>Name</th>
<th>Cylinder number</th>
<th>Lambda</th>
</tr>
</thead>
<tbody>
<tr>
<td>Base line-engine</td>
<td>4</td>
<td>1.33</td>
</tr>
<tr>
<td>Flow control baffle No. 1</td>
<td>2</td>
<td>1.49</td>
</tr>
<tr>
<td>Flow control baffle No. 2</td>
<td>2</td>
<td>1.42</td>
</tr>
</tbody>
</table>

CO emissions are essentially insensitive to changes in ignition timing, as they are almost entirely a function of the A/f ratio. As observed in Fig. 13, The CO emission is not affected in mixture leaner than 1.2.

Although HC emissions mimic CO emissions by falling in response to higher excess air factors in the rich range, the hydrocarbon starts to rise in the lean range. Minimum HC emissions within the lean range occur at roughly lambda = 1.1 … 1.2.

The HC emissions for different control baffles are observed in Fig. 13. The HC emissions of engine with control baffle are higher than base line engine. This matter maybe occurs because of more heat transfer to the engine wall (due to higher rotation) and deeper quench zone that arises from lower combustion chamber temperature.

The relationship between NOx and the excess-air factor (Lambda) is the reverse of the pattern described about HC. In the rich range, NOx emissions respond to higher excess factors and their higher oxygen concentrations by climbing. In the lean range, NOx emissions react to increases in excess air factor by falling, as the progressive reduction in mixture densities results in lower combustion-chamber temperatures.

Maximum NOx emissions are encountered with moderate excess air in the lambda 1.05 to 1.1 ranges.

6. Injection results

The air/fuel ratio distribution for baffle No. 1 is smoother than other configuration and baffle No. 1 has a richest area around the spark (Fig. 16).
Fig. 13. Effect of excess-air factor on CO emission for different configurations.

Fig. 14. Effect of excess-air factor on HC emissions for different configuration.

Fig. 15. Effect of excess-air factor on NOx emissions for different configuration.

The NOx emission for engine with flow control baffle is 246 ppm in $\lambda=1.49$ but it is 912 ppm for standard engine in $\lambda=1.35$.

Fig. 16. Air/fuel ratio for baseline engine (330° CA)

Fig. 17. Air/fuel ratio for baffle no.1 (330° CA)

Fig. 18. Air/fuel ratio for baffle no.2 (330° CA)
7. Injection timing

The consequences of injection timing in terms of cylinder pressures are shown in figs. 19 and 20. It is clear that there is a minimum in the maximum pressure and mean-effective pressures. With the beginning of fuel injection at 300 °CAD to 360 °CAD and 420 °CAD after top-dead-centre of intake and this corresponds to a maximum in the concentration of unburned hydrocarbons as would be expected. The variance of the mean-effective pressure is also a maximum at 360 °CAD after intake and corresponds to a reduction in drivability. With injection over a wide range of crank angles corresponding to closed valves, there is little difference in the performance.

8. Conclusions

This study demonstrates the ability of an inlet system using flow-control baffle to induce swirling and tumbling motions in the four valve engine and to investigate the influence of swirling and tumbling motions in increasing the lean-limit of combustion.

CFD calculation and Flow Bench test rig show that the flow control baffle can change the flow pattern significantly.

Swirling motion can exist until the end of compression cycle but tumble motion is diminished faster, moreover, specific design of flow-control allows evaluating and comparing the potential of different inlet systems concerning engine combustion characteristics.

It is demonstrated the ability of swirling motion to improve engine stability compared to tumbling motion in current engine.

The engine with higher range of rotation ratio has better lean burn capability and this matter is the results of two opposite subjects, negative effect of more heat transfer and positive effects of more turbulence and orderly bulk flow.

The HC emissions of engine with higher flow rotation (swirl or tumble) is higher, because of thicker quench layer, higher heat transfer and larger fuel wet area.

In mass production, the flow control baffle can be replaced with control devices such as swirl control valve or valve deactivation mechanism that can be fully open in full load.

REFERENCES: